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(54) Title: PROCESS FOR PRODUCTION OF POLYOLS, AND POLYOLS FOR POLYURETHANE

(57) Abstract: Polyols useful for preparing foamed polyurethane systems are produced by reacting a feed stock of agricultural origin with a multifunctional hydroxyl component and di basic acids in the presence of a catalytically effective amount of a catalyst suitable to polymerize the agricultural feed stock. The resultant in polyol is then purified and blended with other ingredients to produce a formulated polyol suitable for specific polyurethane foam systems. The polyols produced in accordance with the method are also described.

reacting under agitation a mixture of a predetermined quantity of agricultural feed stock in a ratio of about 100 parts, with a multifunctional hydroxyl component in a ratio of about 10 to about 200 parts. At least one di basic acid, or a mixture of di basic acids, is also added and reacted in the mixture in a ratio of up to about 100 parts. The reaction is conducted in the presence of a free radical catalyst suitable for estrification and polymerization, typically an alkali/alkaline earth/tin based catalyst, in an amount of about 0.01 percent to about 2 percent by weight of the mixture. The reaction is conducted at a temperature and for a time effective to result in a polyol useful for producing polyurethane foam.

In a more specific aspect, the feed stock is vegetable oil, or a mixture of vegetable oils, and more particularly castor oil. Castor oil is a nondrying oil extracted from the castor bean, which after processing, has previously been used as a lubricant among other applications. It is also known as ricinus oil. The reaction is preferably conducted at a temperature of about 150°C to about 250°C. Yet more preferably, the reaction is conducted for a time period of about 6 hours to about 8 hours to result in different polyester polyols of 2 to 5 (hydroxyl) functionality. In conducting the reaction, preferably the hydroxyl component is a multifunctional hydroxyl component such as glycerin and sorbitol.

In another aspect, the invention is directed to a polyol for use in the production of polyurethane foam which is the product of the previously described reaction. More specifically, the polyol results from the reaction in which the feed stock is castor oil with the polyol resulting from having blended the reaction product with stabilizer catalyst and blowing agents to result in a polyol suitable for production of a predetermined polyurethane foam.

Having thus briefly described the invention, the same will become better understood from the following detailed discussion.

### **Detailed Discussion of the Invention**

In accordance with the invention there is provided a process for manufacture of polyols which are useful for manufacturing polyurethane foam. Specifically, the process results in polyester polyols which are prepared from vegetable oils such as castor oil, or other ingredients mostly derived from agricultural sources.

The other vegetable oils considered are unsaturated oils like Soybean oil. Multifunctional hydroxyl components used as one of the reaction input are the substances like

**Example V**

240.6 gms of Castor oil is reacted with 164.1 gms. of a mixture of glycerin using 0.5% of the tin catalyst in a stirred glass reactor at a temperature of 200 to 250° C. for one to two hours. After two hours, 95.3 gms. of Phthalic acid is added and reaction proceeds at 180° C. for the next two hours. Thereafter, the reaction temperature is increased to 220° C. for another two hours to complete the reaction. The reaction is carried out under nitrogen initially, and a vacuum is applied during the last half hour to complete the reaction and to bring the acid value to less than one. The resulting product is a polyol having a functionality of between 4 to 5 and having OH of 470 to 490 MgKOH/gm.

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**Example VI**

146.8 gms. of Castor oil is reacted with 69.29 gms. of a mixture of Adipic and Phthalic acid in a stirred glass reactor at a temperature of 200 to 250° C. for about four hours. Thereafter, 283.9 gms. of peg 600 is added and reaction proceeds further using 0.1% of a tin catalyst at 180° C. to 230° C. for the next 10 to 12 hours. The reaction is carried out under nitrogen initially and vacuum is applied during last three hour to complete the reaction and to bring the acid value less than one. The resulting product is a polyol with a functionality of approximately 3 and having OH of 30 to 50.

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**Example VII**

134.7 gms. of Castor oil is reacted with 211.74 gms. of a mixture of Adipic and Phthalic acid in a stirred glass reactor at a temperature of 200 to 250° C. for about four hours. Thereafter, 153.55 gms. of DEG is added and reaction proceeds further using 0.1% of tin catalyst at 180° C. to 220° C. for next 10 to 12 hours. The reaction is carried out under nitrogen initially and a vacuum is applied during the last three hours to complete the reaction and to bring the acid value to less than one. The resulting product is a polyol with a functionality of between 2 to 3 and having OH of 30 to 45.

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Having thus generally described the invention, the same will become better understood from the following claims in which it is set forth in a nonlimiting manner.

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glycerin and sorbitol. A significant source of glycerin is from saponification vegetable oils like Palm oil, whereas Sorbitol is produced using sucrose as the starting material. Sucrose is fully derived from agricultural sources with multifunctional hydroxyl components to produce a polyester polyol of about 2 to about 5 (hydroxyl) functionality useful for the manufacturer of polyurethane foam. For purposes of this disclosure, it is noted that OH refers to the hydroxyl number of the polyol. The functionality refers to the average number of hydroxyl groups per molecule of polyol and m.w. refers to the molecular weight of the polyol.

The polymer/polyols in accordance with the invention are produced by estrification/trans estrification of a polymerization known quantity of vegetable oil such as castor oil in a mixture with at least one multifunctional hydroxyl component, i.e., OH greater than 1, or a mixture thereof, and di basic acid. The previously mentioned materials are reacted under agitation at a temperature range of about 150°C to about 250°C in the presence of a catalytically effective amount of a conventional free radical catalyst known to be suitable for the polymerization of the unsaturated monomers in the oil. Specifically, such a catalyst can be an alkali/alkaline earth/tin based catalyst in an amount of anywhere from 0.01 to about 2 percent by weight. The reaction is conducted typically for a period of about 2 to about 8 hours to result in a polyol which can then be purified and standardized. More specifically, depending on the specific ratios, temperatures and time of reaction, different polyols of functionality of about 2 to about 5 (hydroxyl) value can be produced.

In a second step, depending on the desired polyurethane foam system to be prepared from the polyols, the polyols can be blended with appropriate ingredients such as a stabilizer catalyst, blowing agents, etc., to produce formulated polyols useful for achieving a desired performance of the polyurethane foam system to be produced. More specifically, the resultant polyols from the process of invention are typically polyesters which are used to produce foam polyurethane systems.

The invention also relates to the polyols produced with accordance with the process described herein.

### **Examples I-VII**

A series of polymer/polyols were prepared in batch processes. Examples I-VII below describe the different types of polyols which result from conducting the process with varying

constituents of the mixtures, and under varying temperature and time conditions to result in different polyols, i.e. polyesters.

**Example I**

5 400 gms. of Soybean oil is reacted with 100 gms. of Glycerin in a stirred glass reactor at a temperature of 200 to 245° C. for three hours in the presence of 0.1% of a tin catalyst. The reaction is carried out in a nitrogen atmosphere. The resulting product is a polyol of functionality of approximately 2 and has OH of 280 to 330 MgKOH/gm.

10 **Example II**

218.35 gms. of Castor oil is reacted with 281.35 gms. of a mixture of diols (peg 600) in a stirred glass reactor at a temperature of 200 to 240° C. for three to four hours in the presence of 0.5% of alkaline earth catalyst. The reaction is carried out in a nitrogen atmosphere. The resulting product is a polyol of functionality of between 2 to 3 and has OH of 170 to 200  
15 MgKOH/gm.

**Example III**

400 gms. of Castor oil is reacted with 100 gms. of glycerin in a stirred glass reactor at a temperature of 200 to 240° C. for three to four hours in the presence of 0.5 to 1% of an  
20 alkaline earth catalyst. The reaction is carried out in a nitrogen atmosphere. The product is purified by precipitating the catalyst chemically and filtering it off. The resulting product is a polyol has a functionality of approximately 3 and has OH of 410 to 450 MgKOH/gm.

**Example IV**

25 364 gms. of Castor oil is reacted with 135.88 gms. of a mixture of glycerin and sorbitol in a stirred glass reactor at a temperature of 200 to 250° C. for three to four hours in the presence of 1% of an alkaline earth catalyst. The reaction is carried out in a nitrogen atmosphere. The resulting product is a polyol, which is then purified by removing the catalyst chemically by precipitating the catalyst and filtering it off. The resulting polyol has a functionality of  
30 between 3 to 4 and OH of 380 to 400 MgKOH/gm.

**Claims**

What is claimed is:

1. A process for the production of polyol for use in production of polyurethane foam, comprising reacting under agitation:
  - 5 a mixture of a predetermined quantity of agricultural origin feed stock in a ratio of about 100 parts, with a multifunctional hydroxyl component in a ratio of about 10 to about 200 parts, and at least one di basic acid in a ratio of up to about 100 parts of the mixture;
  - said reaction being conducted in the presence of a catalyst suitable for  
10 polymerization in an amount of about 0.01 percent to about 2 percent by weight of the mixture; and
  - said reaction conducted at a temperature and for a time effective to result in a polyol useful for producing polyurethane foam.
- 15 2. The process of claim 1, wherein said feed stock is at least one vegetable oil.
3. The process of claim 2, wherein said vegetable oil includes castor oil.
4. The process of claim 1, wherein said reaction is conducted at a temperature of  
20 about 150° C to about 250° C.
5. The process of claim 1, wherein said hydroxyl component comprises glycerin.
6. The process of claim 1, further comprising conducting said reaction at a  
25 temperature and for a time effective to result in a polyester polyol of about 2 to about 5 (hydroxyl) functionality.
7. The process of claim 1, further comprising conducting said reaction at a temperature of about 150° C to about 250° C for about 6 to 8 hours.
- 30 8. The process of claim 1, further comprising blending the resultant polyol with

15. The polyol of claim 10, wherein said polyol comprises a polyol of about 2 to about 5 (hydroxyl) functionality.

16. The polyol of claim 10, wherein the polyol results from having conducted said  
5 reaction at a temperature of about 150° C to about 250° C for about 6 to about 8 hours.

17. The polyol of claim 10, wherein the polyol results from having blended the  
reaction product with stabilizer catalyst and blowing agents to result in a polyol suitable for  
production of a predetermined polyurethane foam.

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18. The polyol of claim 17, wherein the polyol results from having purified the  
reaction product before conducting said blending.

stabilizer catalyst and blowing agents to result in a polyol suitable for production of a predetermined polyurethane foam.

9. The process claim 8, further comprising purifying the resultant polyol before  
5 conducting said blending with stabilizer catalyst and blowing agents.

10. A polyol for use in production of polyurethane foam comprising the product of a reaction under agitation of:

a mixture of a predetermined quantity of agricultural origin feed stock in a  
10 ratio of about 100 parts, with a multifunctional hydroxyl component in a ratio of about 10 to about 200 parts, and at least one di basic acid in a ratio of up to about 100 parts of the mixture; and

the reaction having been conducted in the presence of a catalyst suitable for polymerization in an amount of about 0.01 percent to about 2 percent by weight of the  
15 mixture; and

the reaction having been conducted at a temperature and for a time effective to result in the polyol useful for producing polyurethane foam.

11. The polyol of claim 10, wherein the polyol results from the reaction in which  
20 the feed stock includes castor oil.

12. The polyol of claim 10, wherein the polyol results from the reaction in which the feed stock is at least one vegetable oil.

25 13. The polyol of claim 10, wherein the polyol results from the reaction in which the hydroxyl component in the reaction comprises glycerin.

14. The polyol of claim 10, wherein the polyol results from having conducted the reaction at a temperature of about 150° C to about 250° C.



INTERNATIONAL SEARCH REPORT

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**A. CLASSIFICATION OF SUBJECT MATTER**  
 IPC(7) :C09F 7/06, 7/10; C11B 3/00, 7/00; C08G 18/68  
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 According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)  
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Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	CA 2,144,467A1 (SCHOLL et al) 18 September 1995, example 1; page 5, line 6; table, page10.	1-18

Further documents are listed in the continuation of Box C.  See patent family annex.

* Special categories of cited documents:	"T"	later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"A" document defining the general state of the art which is not considered to be of particular relevance	"X"	document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
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"O" document referring to an oral disclosure, use, exhibition or other means		
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